

# ***Separations of Actinide Elements***

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*Workshop for Graduate Students from the  
Big 10 Nuclear Engineering Departments*

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# ***Actinide Separations***

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- **Why are they needed?**
  - Can address major technical, social and political issues related to disposal of nuclear wastes
  - Regulatory requirements associated with actinide waste disposal are more stringent than those for other radioactive wastes
    - *Waste present a greater health hazard*
    - *Isotopes have long half lives*
- **Sources of actinides**
  - “Legacy waste” from weapons production
  - Spent nuclear fuel
  - Medical and industrial isotope production wastes

# Actinides Are Separated from What?

- Mainly from
  - Each other

	90	91	92	93	94	95	96	97	98	99	100	101	102	103
<b>Actinide Series~</b>	<u>Th</u>	<u>Pa</u>	<u>U</u>	<u>Np</u>	<u>Pu</u>	<u>Am</u>	<u>Cm</u>	<u>Bk</u>	<u>Cf</u>	<u>Es</u>	<u>Fm</u>	<u>Md</u>	<u>No</u>	<u>Lr</u>
	232.0	(231)	(238)	(237)	(242)	(243)	(247)	(247)	(249)	(254)	(253)	(256)	(254)	(257)

- Lanthanides (also known as Rare Earths)

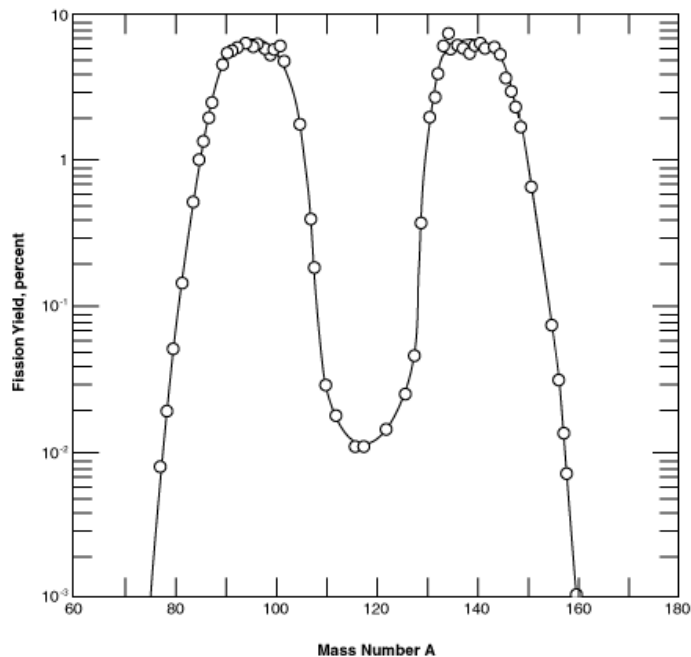
	58	59	60	61	62	63	64	65	66	67	68	69	70	71
<b>Lanthanide Series*</b>	<u>Ce</u>	<u>Pr</u>	<u>Nd</u>	<u>Pm</u>	<u>Sm</u>	<u>Eu</u>	<u>Gd</u>	<u>Tb</u>	<u>Dy</u>	<u>Ho</u>	<u>Er</u>	<u>Tm</u>	<u>Yb</u>	<u>Lu</u>
	140.1	140.9	144.2	(147)	150.4	152.0	157.3	158.9	162.5	164.9	167.3	168.9	173.0	175.0
<b>Actinide Series~</b>	<u>Th</u>	<u>Pa</u>	<u>U</u>	<u>Np</u>	<u>Pu</u>	<u>Am</u>	<u>Cm</u>	<u>Bk</u>	<u>Cf</u>	<u>Es</u>	<u>Fm</u>	<u>Md</u>	<u>No</u>	<u>Lr</u>
	232.0	(231)	(238)	(237)	(242)	(243)	(247)	(247)	(249)	(254)	(253)	(256)	(254)	(257)

# Actinides Are Separated from What?

- From other fission products

*Fission products with mass numbers around 90 and 140 have particularly high fission yields*

Thermal Neutron Fission of U-235



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37 <u>Rb</u> 85.47	38 <u>Sr</u> 87.62	39 <u>Y</u> 88.91	40 <u>Zr</u> 91.22	41 <u>Nb</u> 92.91	42 <u>Mo</u> 95.94	43 <u>Tc</u> (98)	44 <u>Ru</u> 101.1	45 <u>Rh</u> 102.9	46 <u>Pd</u> 106.4	47 <u>Ag</u> 107.9	48 <u>Cd</u> 112.4	49 <u>In</u> 114.8	50 <u>Sn</u> 118.7	51 <u>Sb</u> 121.8	52 <u>Te</u> 127.6	53 <u>I</u> 126.9	54 <u>Xe</u> 131.3
55 <u>Cs</u> 132.9	56 <u>Ba</u> 137.3	57 <u>La*</u> 138.9															

# What are the Actinides of Most Interest?

- **Those with a low atomic-number**
  - Elements beyond Cm are present in very low concentrations
    - *Produced only under highly specialized circumstances*
- **Those that are alpha-emitters**
  - Radium and radon are decay daughters of actinides

Isotope	Atomic No.	Half Life
Ra-226	88	1.6E+03 y
Rn-222	86	3.83 d

Isotope	Atomic No.	Half Life
U-232	92	69.8 y
U-233		1.59E+05 y
U-234		2.46E+05 y
U-235		7.04E+08 y
U-238		4.47E+09 y
Np-237	93	2.14E+06 y
Pu-238	94	87.7 y
Pu-239		2.41E+05 y
Pu-240		6.56E+03 y
Pu-242		3.74E+05 y
Am-241	95	4432.7 y
Am-242m		141 y
Am-243		7.36E+03 y
Cm-243	96	30 y
Cm-244		18.1 y
Cm-245		8.5E+03 y
Cm-246		4.73E+03 y



# **Non-technical Issues Associated with Actinide Separations**

- **Primary applications are nuclear power generation and weapons production**
  - Because the technology can be applied to the production of weapons strict controls are imposed due to proliferation risks
    - *Material accountability*
    - *Safeguards and security*
  - From an R&D perspective these controls add a layer of complexity that does not exist in other separation applications

# ***Technical Challenges to Actinide Separations***

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- **Concentrations in either spent fuel or in tank HLW will vary widely**
  - Must design separation processes robust enough for a wide range of feeds
  - Feed characterization requires significant analytic capability
- **Concentrations in feeds are very dilute**
  - Low concentrations in spent fuel (except for U)
  - Early nuclear area waste management approach was based on dilution and dispersal
- **Chemistry of actinides is complex**
  - Actinides form multiple valence states
  - Similar to that of lanthanides

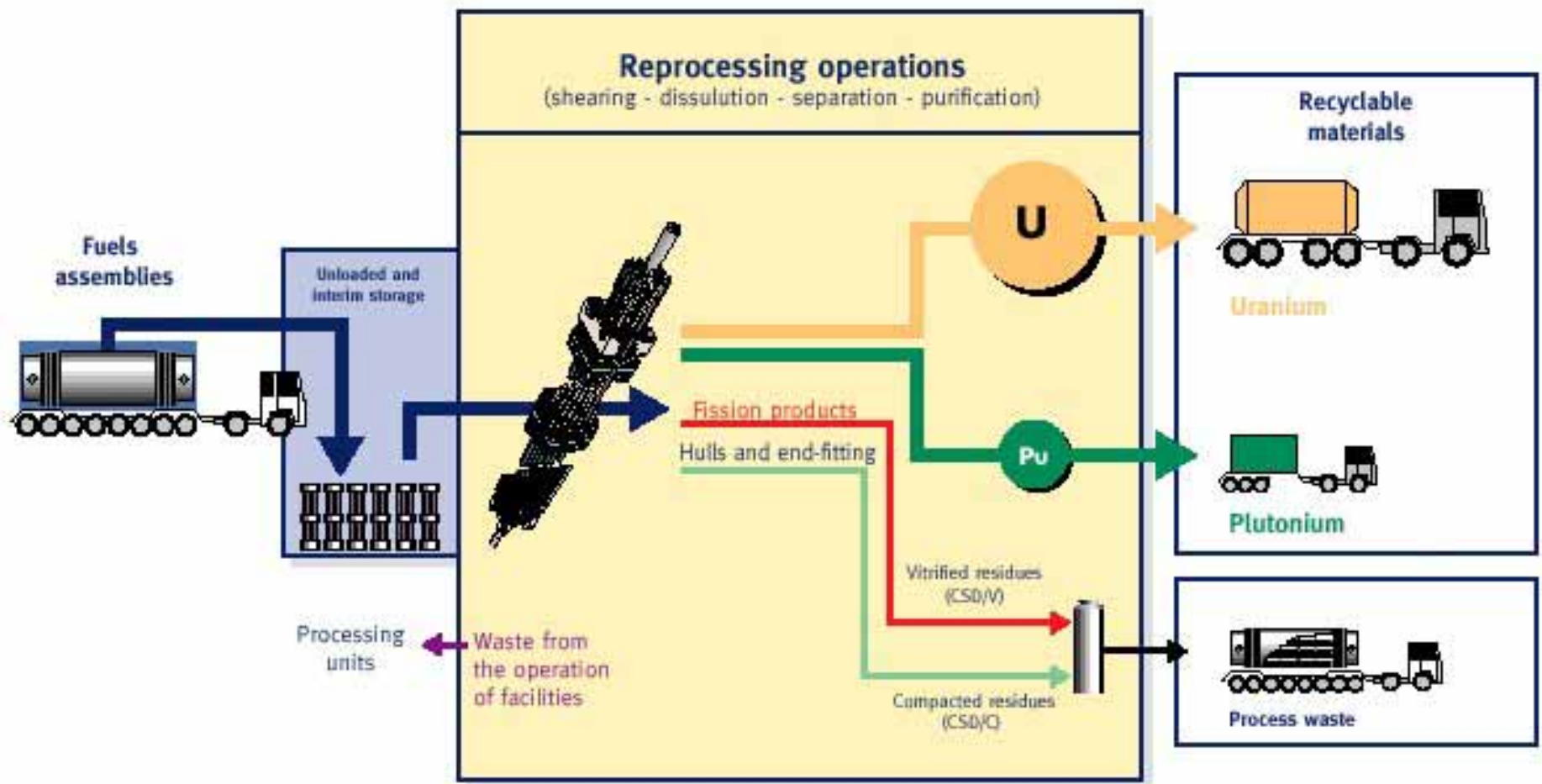
# ***State of the Art in Actinide Separation***

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- **Aqueous based processes**
  - **Liquid-liquid extraction**
  - Precipitation
  - Ion exchange
  - Membranes
  - Crystallization
  - Supercritical fluid extraction
- **Dry processes**
  - **Pyroprocessing**
    - ***Electrorefining***
    - ***Oxide reduction***
  - Volatilization
- **Others**



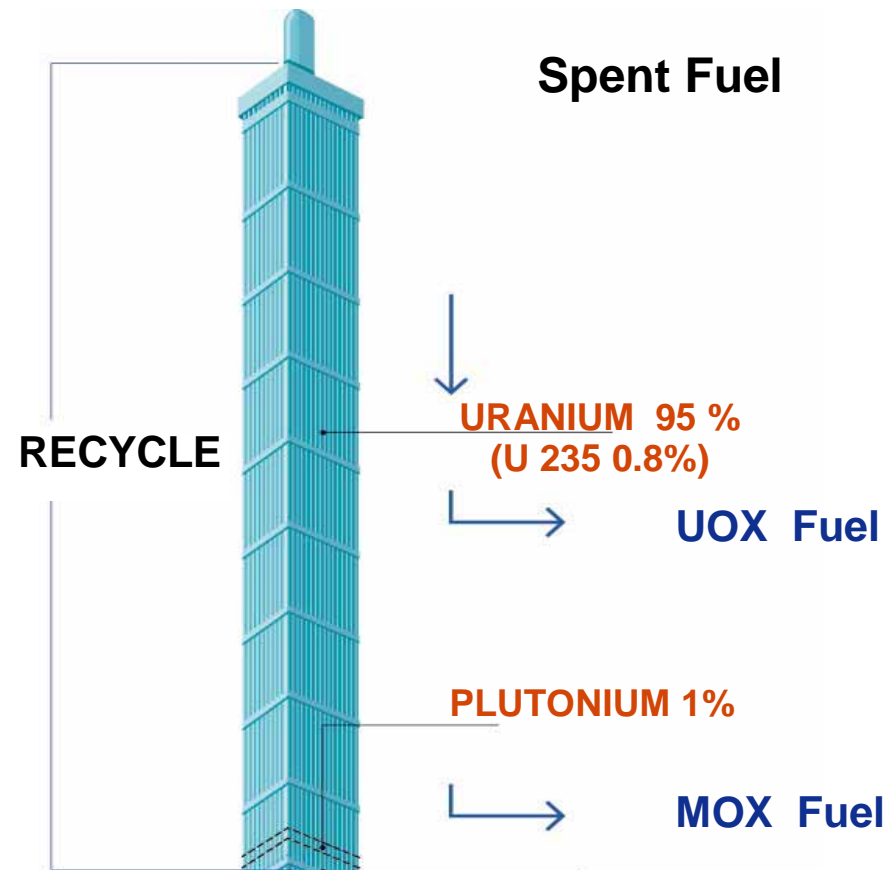
# Actinide Separation – Fuel Cycle



Slide courtesy of COGEMA

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## Spent Fuel Contains 96% Recyclables



Slide courtesy of COGEMA

# ***Actinide Separations Capabilities at ANL***

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*ANL research on actinide separations dates back to the late 1940s*

- **Liquid-liquid extraction**
- **Pyrochemical processing**
- **Spent fuel treatment**
- **TRU, high and low-level waste treatment**
- **Trace analysis of radionuclides**



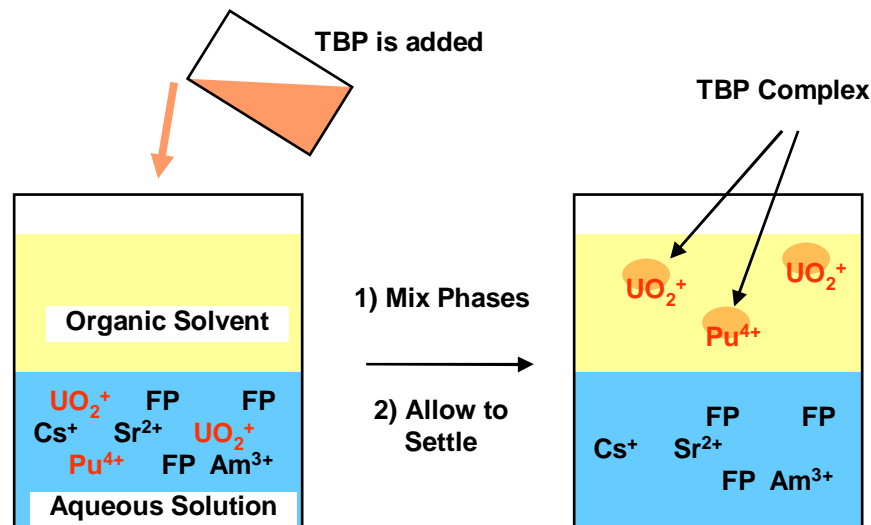
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# *Liquid-liquid Extraction*



# Solvent Extraction Principle

- **Based on relative stability of a metal species in two immiscible liquids**
  - The metal to be separated is contacted with both liquids and is partitioned into each at a constant ratio (the distribution coefficient)
- **Multiple extractions**
  - Not always possible to remove 100% metal with one contact.
  - Options are to greatly increase amount of solvent volume or to use multiple contacts



# ***Solvent Extraction Equipment***

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- **Centrifugal Contactors**

- Short residence time protects solvent from radiolysis and hydrolysis degradation
- High efficiency
- High throughput
- Step-wise phase contact
- Compact unit
- Quickly reaches steady state

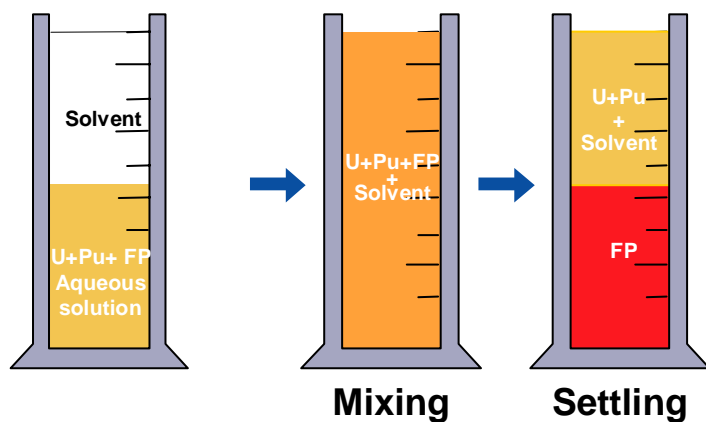
- **Mixer-settlers**

- Long residence time
- Step-wise phase contact
- Extraction combined with reaction

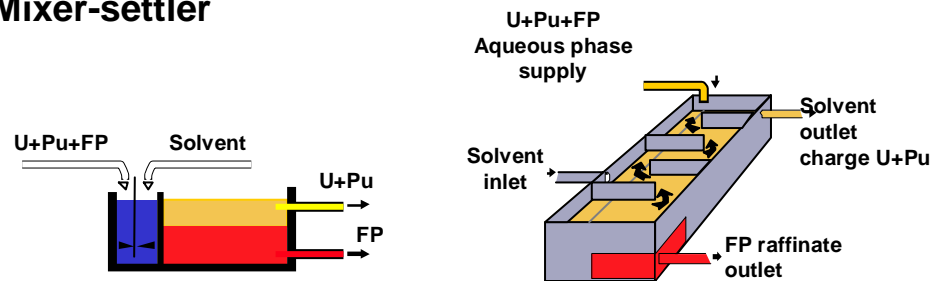
- **Pulsed Columns**

- Long time to reach steady state
- Products with low density difference, low interfacial tension or having a tendency to form emulsions
- High throughput

# Solvent Extraction Equipment

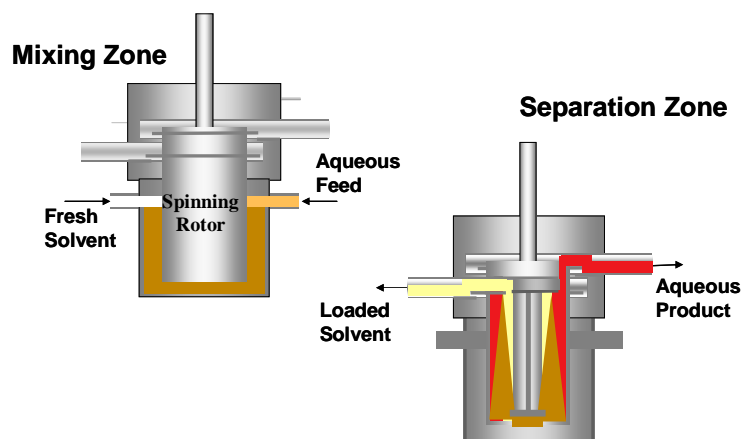


**Mixer-settler**

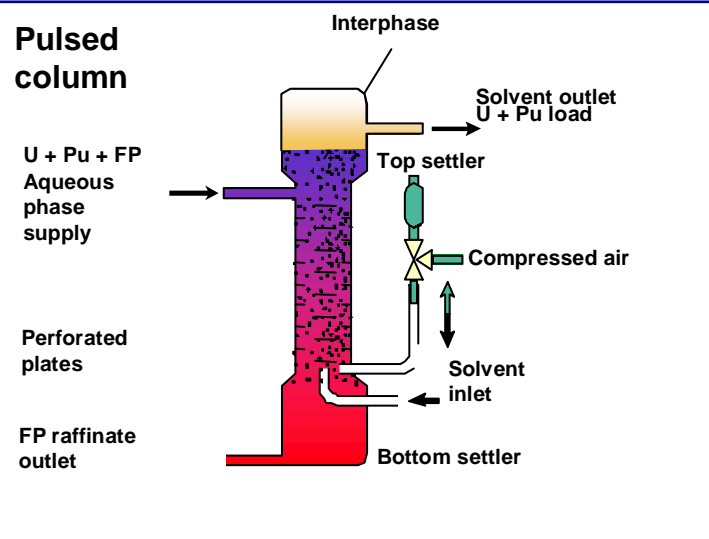


Figures courtesy of ANL and COGEMA

**Centrifugal Contactor**



**Pulsed column**



# ***ANL Solvent Extraction Expertise***

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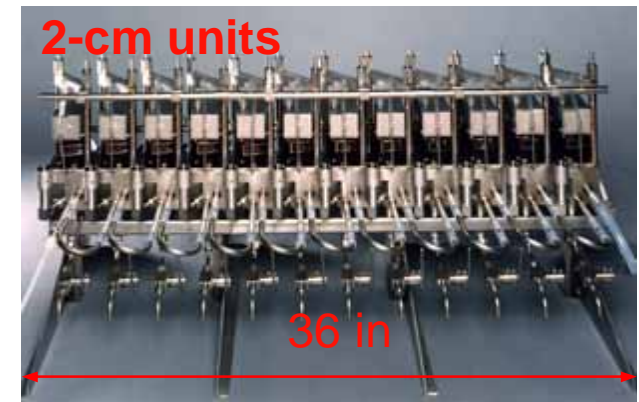
- **Equipment design**
- **Process modeling and design**
- **Process demonstration**





# Equipment Design - ANL Centrifugal Contactor

## Pilot-scale Centrifugal Contactors



Rotor Diameter cm	Nominal Throughput L/min
2	0.04
4	0.4
9	10
10	12
12	20
25	120

→ 0.65 t/d

# ***Process Design and Modeling - AMUSE***

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- The **A**rgonne **M**odel for **U**niversal **S**olvent **E**xtraction—**AMUSE** is a tool we use to:
  - Design and optimize solvent extraction flowsheets
    - *PUREX, UREX, TRUEX, SREX*
  - Perform sensitivity analysis to determine key process variables and their control bound
    - *Flow rates, number of stages, concentration of feed components, concentration of solvent, temperature*

# AMUSE - General Input Form

**AMUSE**

Update Print Run AMUSE  
Verify Input Save Quit

General | Stream Identity | Section 1 | Flowsheet Display

User-specified file name:

Directory (folder) name:

Number of sections:

Process Temperature:

Type of solvent:

- ☒ UREX
- ☐ PUREX
- ☐ TRUEX-NPH
- ☐ TRUEX-TCE
- ☐ TRUEX-SREX
- ☐ TRUEX-DAAP-SREX

Solvent Extraction Type

- ☒ Contactor
- ☐ Pulsed Column
- ☐ Mixer Settler

TBP Concentration:

Recycle Organic

- ☐ Yes
- ☒ No

**Solvent** **Feed** **Scrub** **Strip**

**Extraction** **Scrub** **Strip**

**Raffinate** **Product** **Spent Solvent**

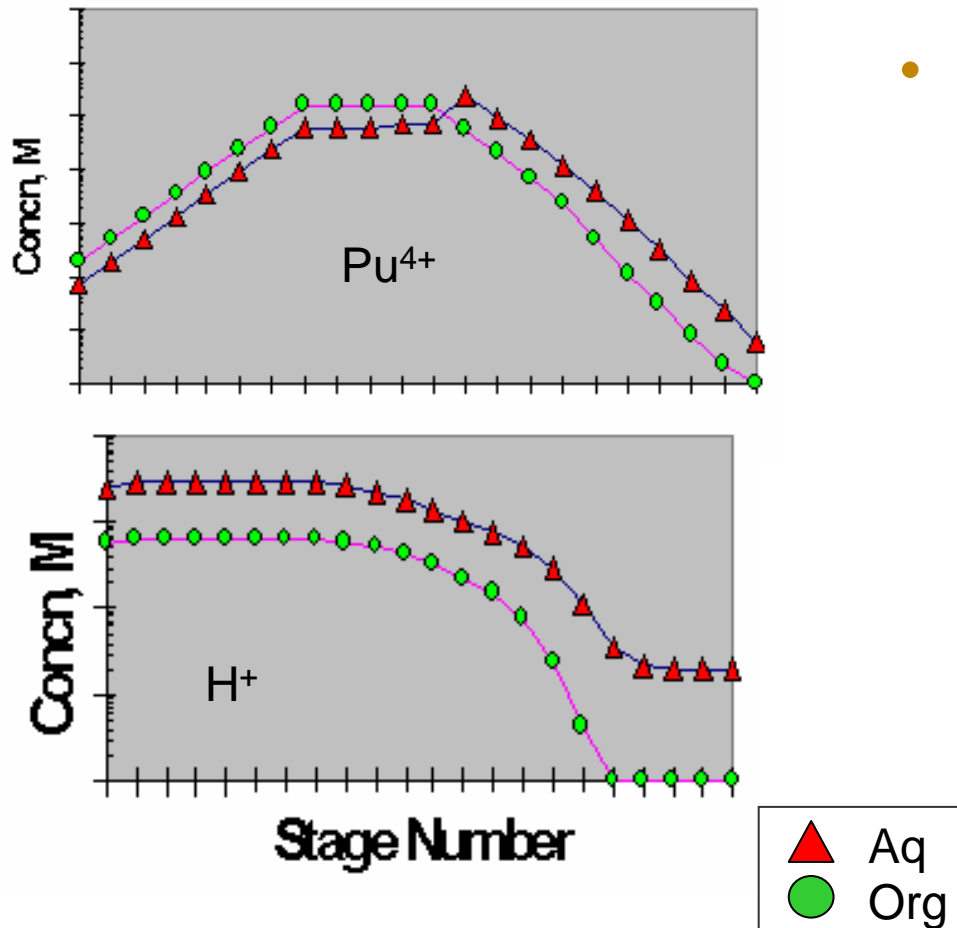
The image displays the AMUSE software interface for the General Input Form. The form includes fields for file name, directory, number of sections, and process temperature. It also features radio button options for solvent type (UREX, PUREX, TRUEX variants), solvent extraction type (Contactor, Pulsed Column, Mixer Settler), and recycle organic status. A process flowchart is shown below the form, illustrating the sequence of operations: Solvent, Feed, Scrub, and Strip. The Scrub and Strip operations are further detailed as Extraction, Scrub, and Strip, leading to the final products: Raffinate, Product, and Spent Solvent.

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# AMUSE – Results

## GRAPHICAL

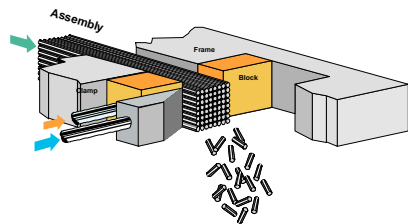


## TABULAR

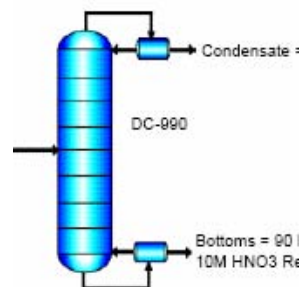
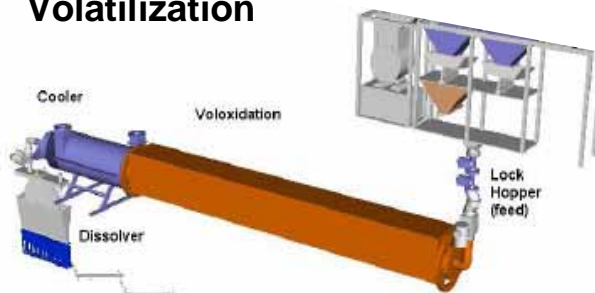
- **Tabular reports are created for**
  - Influent and effluent compositions and flow rates
  - Stage profiles that include
    - *Distribution ratios*
    - *Component concentrations in organic and aqueous phases*

# Aqueous Spent Fuel Treatment Facility

## Chopping

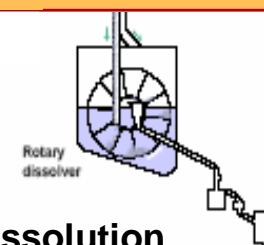
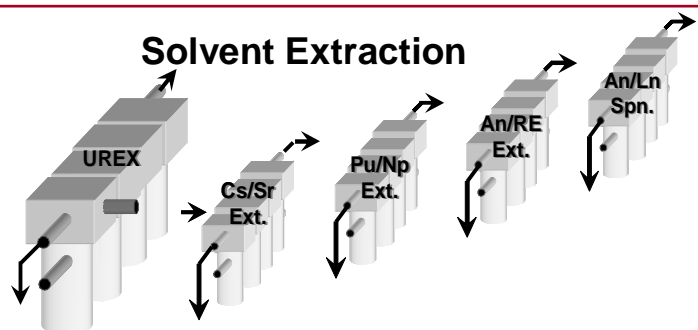


## Volatilization

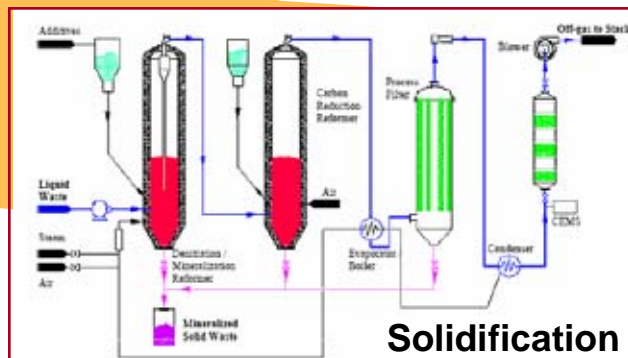


## Concentration

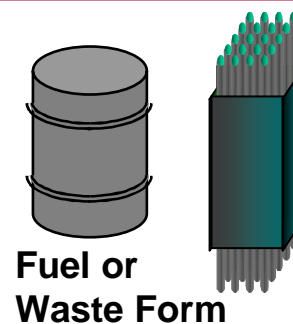
## Solvent Extraction



## Dissolution



## Solidification



## Fuel or Waste Form

Figures courtesy of ANL  
WGI and COGEMA

# ***Process Demonstration – UREX+***

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- **Process being developed as part of the Advanced Fuel Cycle Initiative (AFCI)**
- **Objective:**
  - Demonstrate that all desired spent fuel constituents can be separated to meet required specifications by aqueous processing
- **ANL work is centered on process design, modeling, and demonstration**

# ***Process Demonstration – UREX+***

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- **Spent fuel dissolution**
- **Aqueous based separations:**
  - A series of five solvent-extraction process which separates spent fuel into six product and waste streams
    - $\text{U}_3\text{O}_8$  for recycle or disposal as LLW
    - Np/Pu for mixed oxide fuel for thermal reactors
    - Tc and I for immobilization as HLW
    - Am/Cm for fast-reactor fuel
    - Cs/Sr for decay storage
    - Mixed fission products for repository disposal



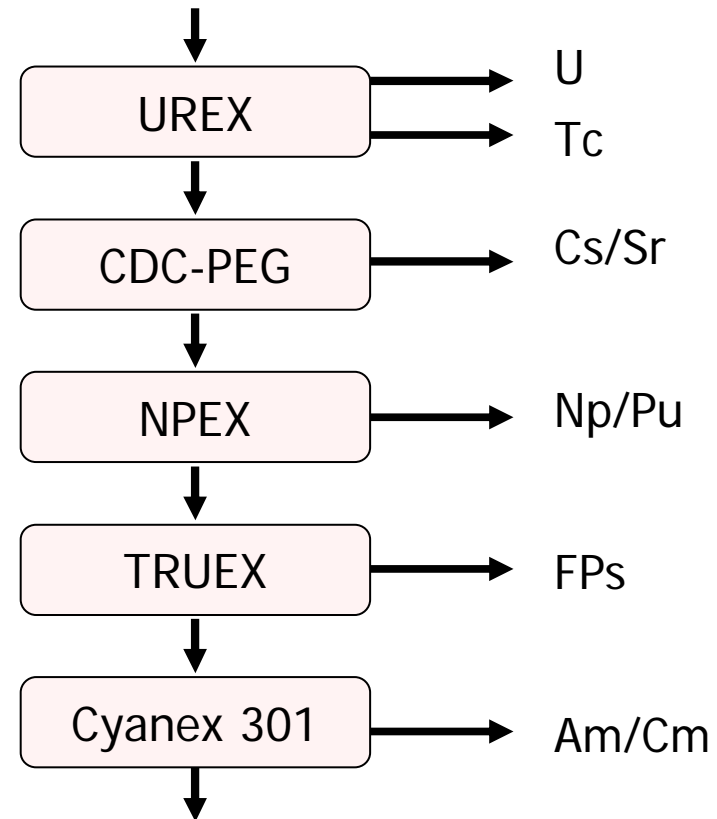
# Process Demonstration – UREX+

- **Flowsheets**

- Developed using the AMUSE code

- **Equipment**

- Three ANL-designed 2-cm contactors were used, set up in a shielded cell, a glovebox, and a vacuum-frame hood
- Can process ~2 kg/day spent fuel (heavy metal)





# Process Demonstration – UREX+ Spent Fuel Dissolution

ANL-designed 2.25 L  
304L SS pressure vessel

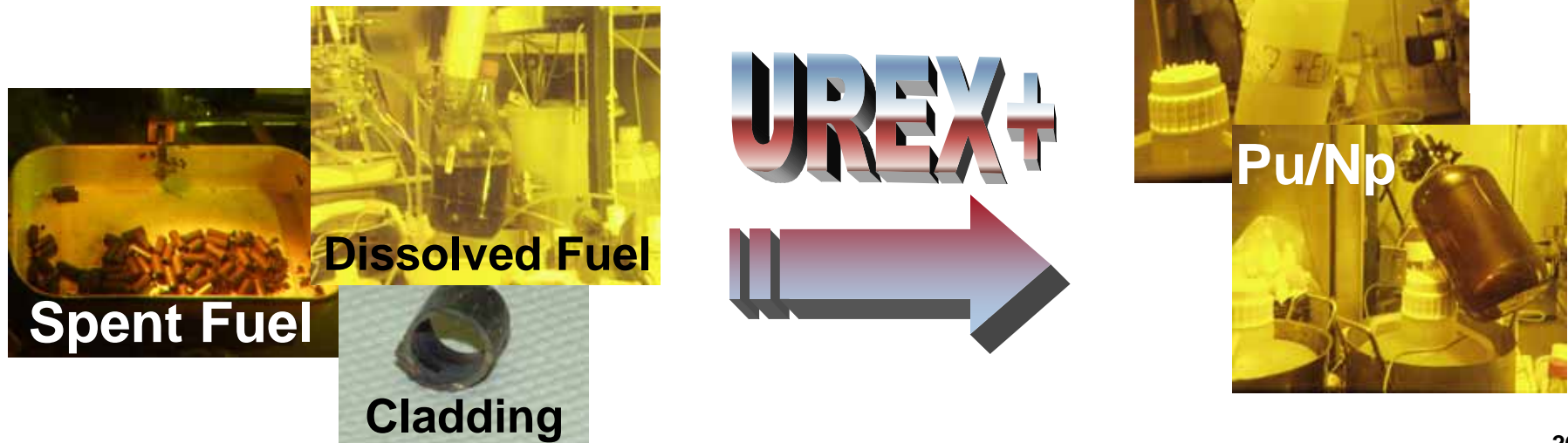
- $\text{UO}_2$  was completely dissolved
- Cladding hulls were very clean
- Sludge was minimal and easily filtered
- Solution was stable



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# Process Demonstration – UREX+ Results

- All processes show high promise for meeting process goals
  - Disposal of uranium as class C LLW
  - Technetium fissile content
  - Pu/Np MOX fuel fabrication
  - Disposal of Cs/Sr as LLW
- Excellent selectivity for the desired products demonstrated for all processes



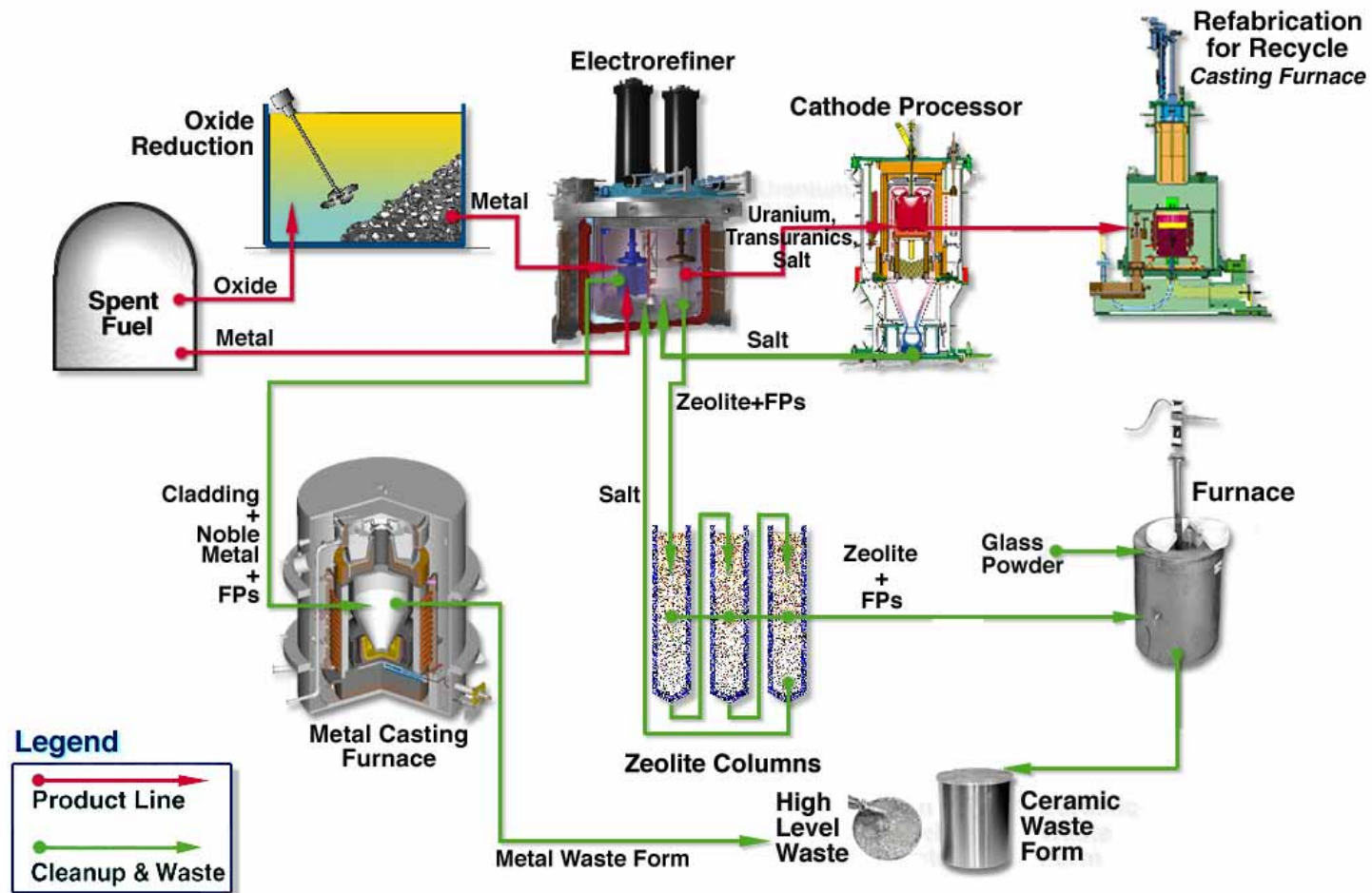
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# *Pyroprocessing*



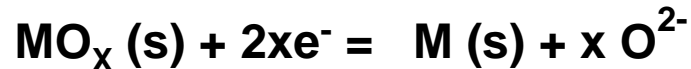
# Pyroprocessing Oxide Fuel



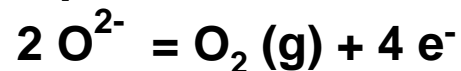
# Oxide Reduction Process

- Goal - develop a commercially viable process for reducing spent fuel oxides to metals
  - High product quality
  - High throughput
  - Simple engineering

- Cathode process



- Anode process





# ***Oxide Reduction Cell and Product***

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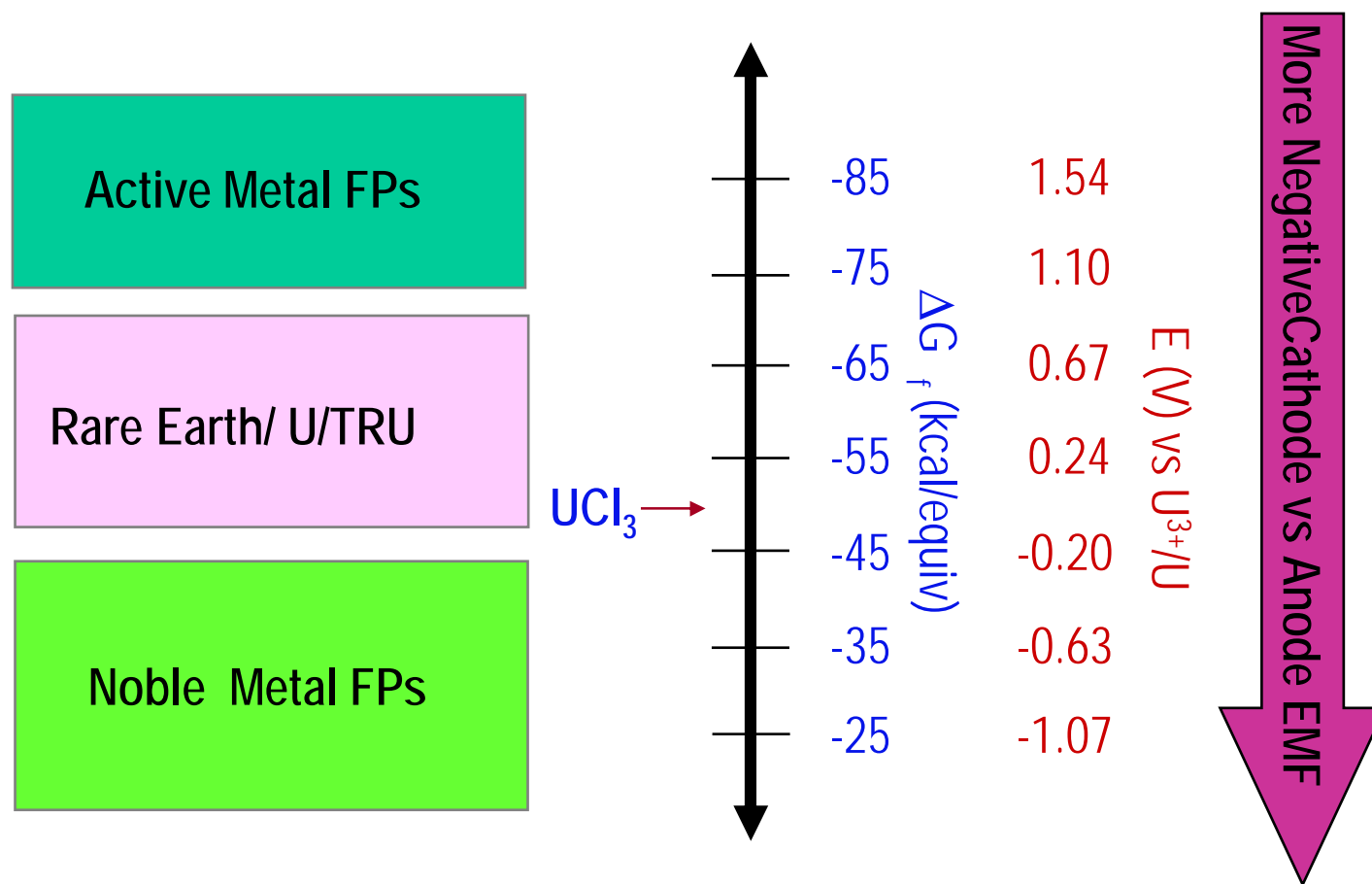
# ***Why Electrorefine Uranium***

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- **Separate uranium from spent nuclear fuel for recycle or disposal as LLW**
  - EBR-II (metal)
  - LWR fuel (oxide)

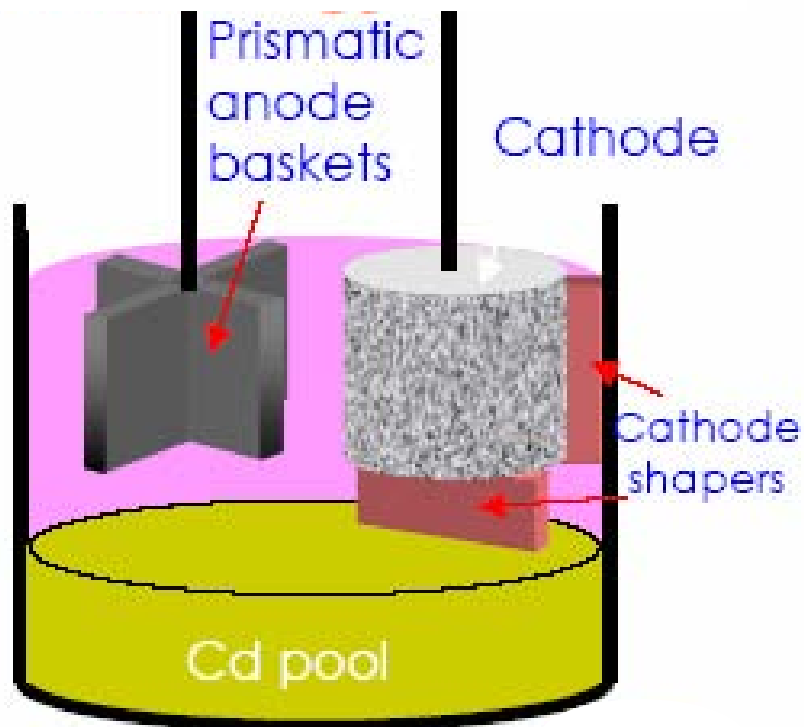


# Thermodynamic Basis





# Pyroprocessing Equipment - Electrorefiner



**Mk-V ACM - Anode Assembly**



**Engineering-Scale Electrorefiner**

# ***ANL Pyroprocessing Expertise***

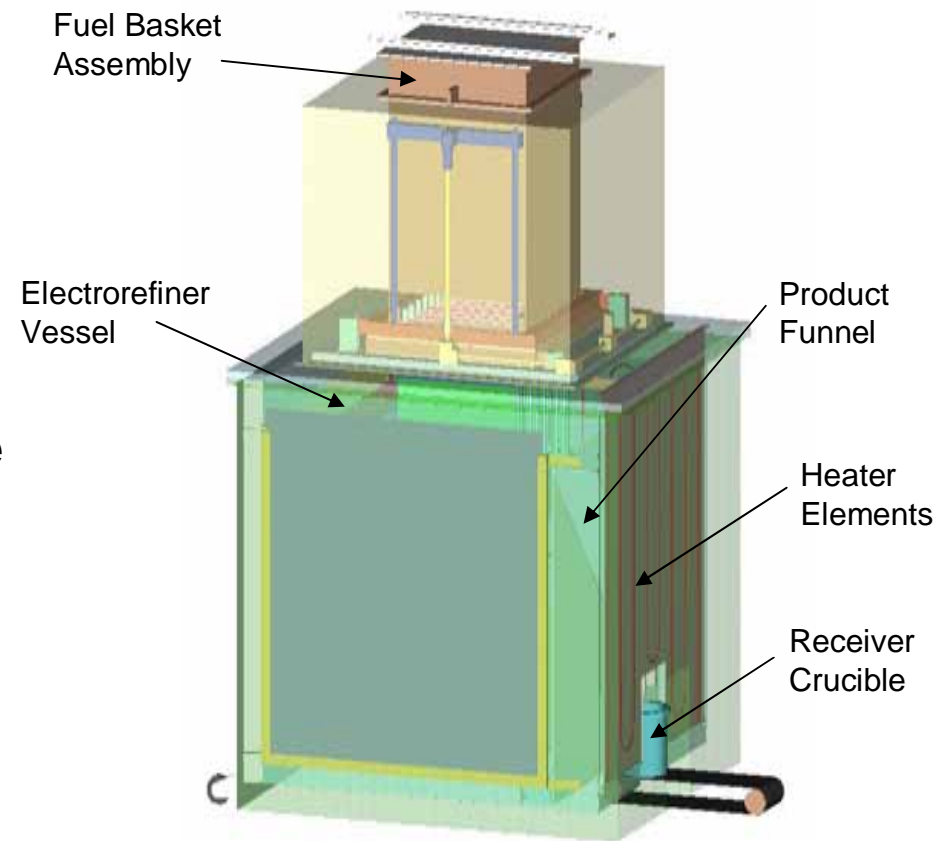
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- **Equipment design**
- **Process modeling and design**
- **Process demonstration**



# Equipment Design

- High throughput electrorefiner
- Electrolytic oxide reduction
- Pyro-contactors
- Liquid cadmium cathode
- Cathode processor
- Metal waste form casting furnace
- Pressureless consolidation for ceramic waste forms



**High Throughput Electrorefiner Prototype**

# ***Process Design***

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***Integration of unit operations to provide an economical recycle process for commercial oxide fuel treatment***

- **Develop a process flowsheet for an integrated pyroprocess oxide-fuel recycle facility**
  - Reference-case throughput of 100 tonne/yr of initial heavy metal
- **Prepare overall requirements to encompass:**
  - Individual operations
  - Facility layout
  - Mechanical and electrical equipment design
  - Maintenance and safeguarding
- **Generate conceptual designs of the facility and the individual pieces of equipment**

# ***Process Modeling***

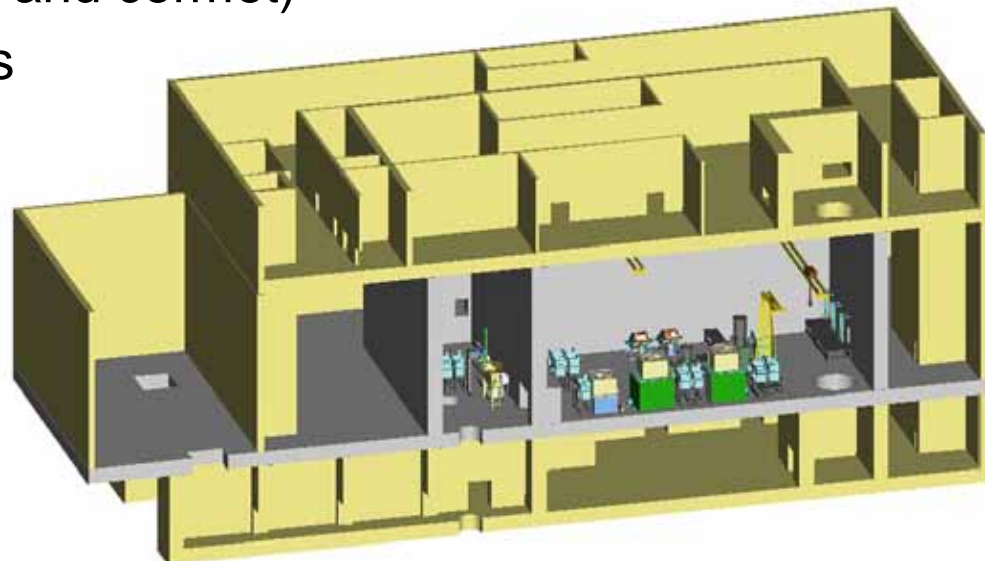
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- **Optimize facility using the operations model**
  - Evaluate equipment layout to minimize materials transfer, to simplify access to services, and to optimize equipment spacing
  - Verify facility design for throughput requirements
  - Identify design shortcomings
  - Provide efficiency data on resources
  - Determine operational bottlenecks
  - Test proposed changes for effectiveness
  - Provide equipment utilization data
- **Assess moving from batch operations to semi-continuous operations**
- **Develop an operations model of the facility**
- **Specify control interface requirements**

# ***Process Demonstration - PYROX***

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- **Process for the treatment of spent light water reactor fuels to recover actinides**
  - Recycle in advanced nuclear reactors
  - Stabilize fission products for repository storage
- **Flowsheets and proof-of-concept tests for treatment of**
  - Dispersion fuels (cercer and cermet)
  - Carbide and nitride fuels
  - Particle fuels



**3-D Schematic of PYROX Facility**

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## ***Other ANL Capabilities Related to the Fuel Cycle***

# ***ANL Capabilities Related to the Fuel Cycle***

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- **Separations**
- **Repository testing and modeling**
- **Materials engineering**
- **Domestic nuclear event attribution**
- **Hydrogen production**

